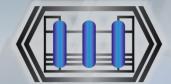
NEW PROJECTS BASED ON TECHNOLOGIES OF PJSC SIE NEFTEHIM FOR PRODUCTION OF HIGH-QUALITY MOTOR GASOLINES

A.S.



JSC SIE NEFTEHIM

Joint Stock Company Scientific Industrial Enterprise Neftehim

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CURRENT TRENDS OF MOTOR GASOLINE PRODUCTION

Share of high-octane gasolines according to EURO-5 standards with content of <u>aromatic hydr</u>ocarbons < 35 vol. % and benzene < 1.0 vol. % is increased

New EURO-6 standards with content of aromatic hydrocarbons < 25 vol. % and benzene < 0.8 vol. % are appeared

Demand of high-octane motor gasoline non-aromatic components (isomerates and alkylates) is enlarged

It is required to decrease share of reformates – high-octane aromatic concentrates

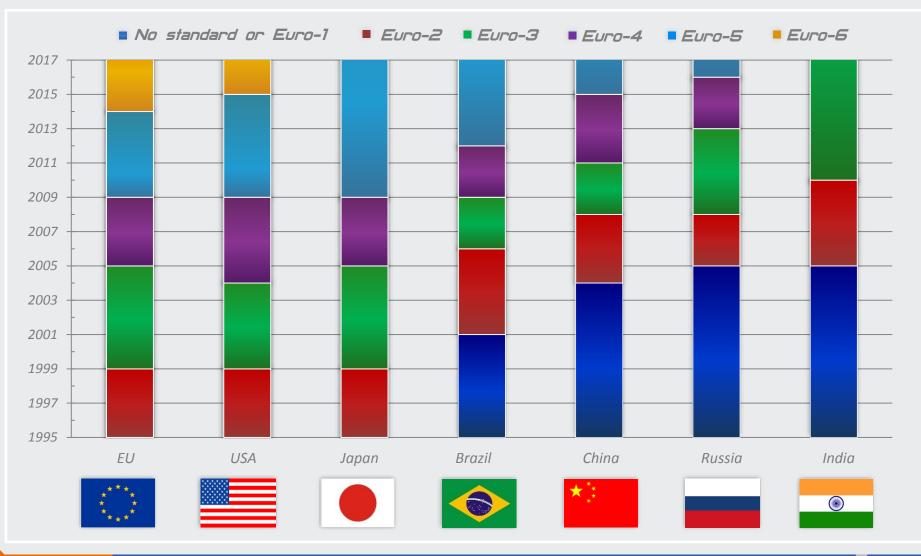
NEW HORIZONS OF MOTOR GASOLINE QUALITY

Performances	EURO-2	EURO-3	EURO-4	EURO-5	EURO-6*
Standard's date of validity in European Union	1995	1999	2005	2009	2015
Standard's date of validity in Russian Federation	2005	2008	2013	2016	-
Date of production termination in Russian Federation	till 01.01.2013	till 01.01.2015	till 01.01.2016	-	-
Benzene content, wt. %, no more than	5.0	1.0	1.0	1.0	0,8
Sulfur content, ppm, no more than	500	150	30	10	10
Aromatic hydrocarbons content, % vol., no more than	-	42	35	35	24
<i>Olefinic hydrocarbons content, % vol., no more than</i>	-	18	14	14	11
Oxygen content, % wt., no more than	-	2.7	2.7	2.7	2.7
Availability of detergent additives	-	Obligatory	Obligatory	Obligatory	Obligatory
NOx emissions, g/kW·h	8.0	5.0	3.5	2.0	0.4

* Performances of motor gasoline according to EURO-6 standard are not definitively established



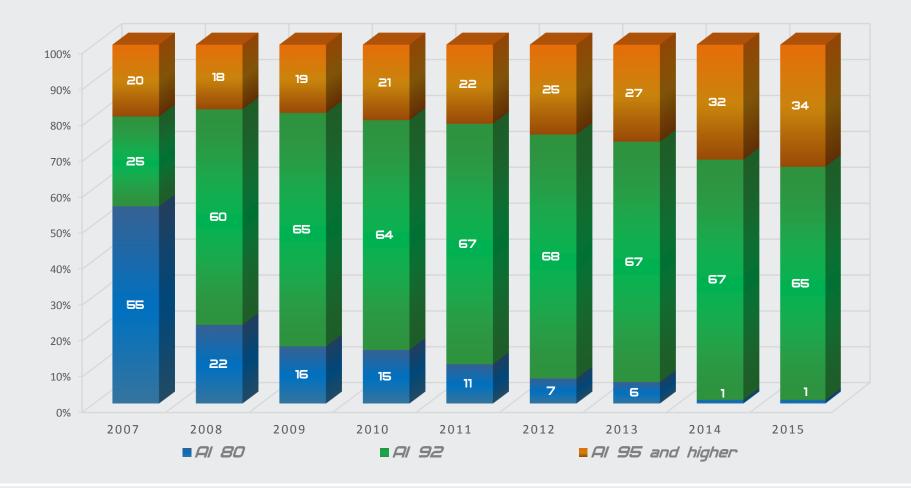
EURO-STANDARDS' IMPLEMENTATION DATE



CHANGE OF MOTOR GASOLINE PRODUCTION STRUCTURE BY CLASSES IN RUSSIA OVER A PERIOD OF 2007-2015



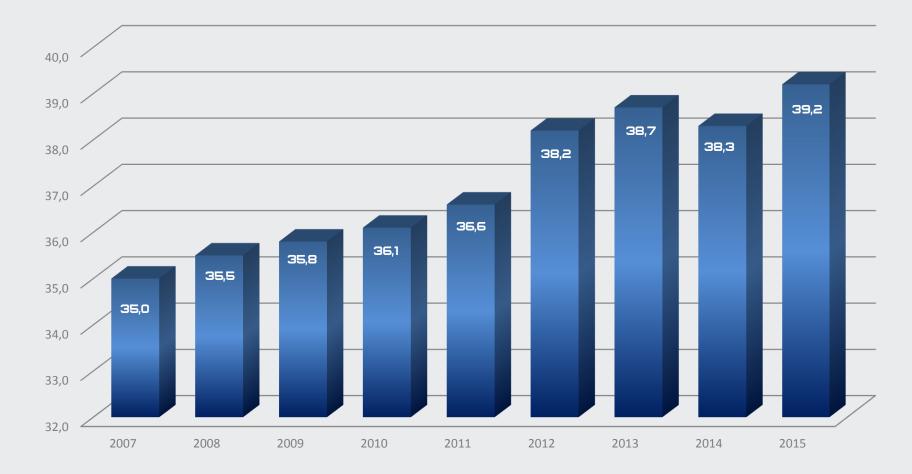
MOTOR GASOLINE PRODUCTION STRUCTURE BY GRADES (RON) IN RUSSIA



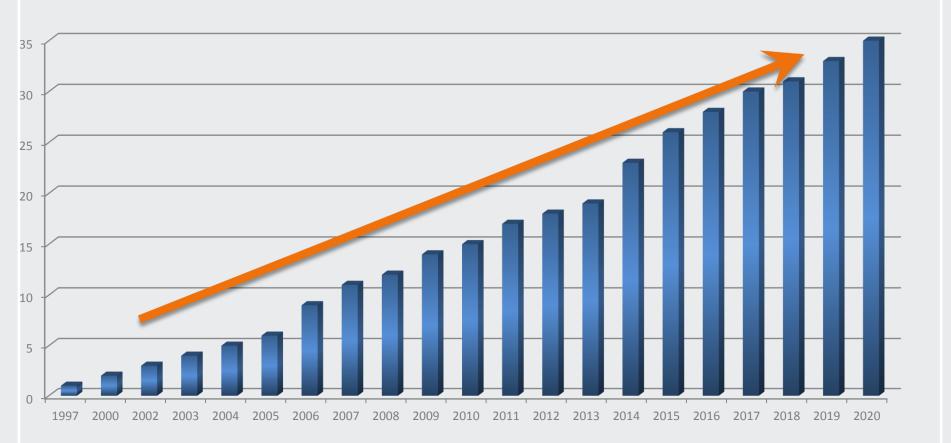


DYNAMICS OF MOTOR GASOLINE PRODUCTION CHANGES IN RUSSIA

MOTOR GASOLINE PRODUCTION IN RUSSIA, MILLION OF TONNES



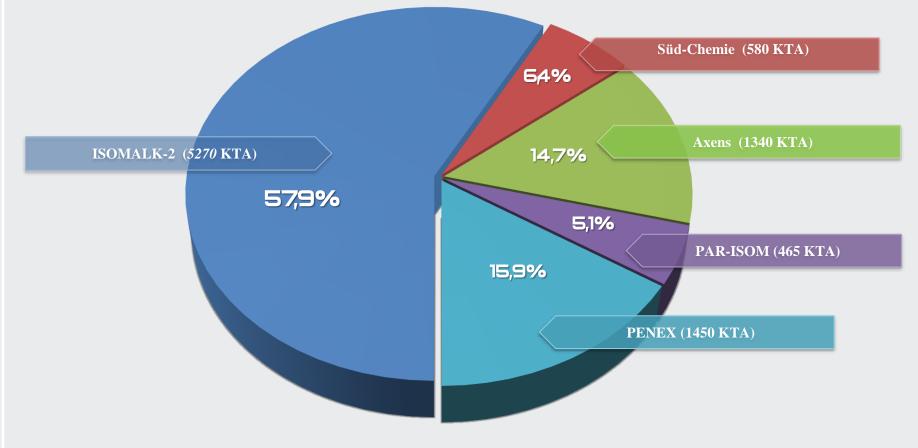
DYNAMICS OF C_s-C_6 ISOMERIZATION UNITS COMMISSIONING IN RUSSIA





SHARE OF DIFFERENT TECHNOLOGIES FOR PRODUCTION OF C_5-C_6 ISOMERATE IN RUSSIA









ISOMERIZATION

Isomerization is the main way to increase share of high-octane motor gasolines according to the standards EURO-5 and EURO-6

- Competitive capacity of isomerization over zeolite catalysts has been dropped sharply. There are two competitive low-temperature isomerization technologies in the world market: over highly-chlorinated alumina catalysts and over sulfated zirconia catalysts:
- Increasingly refiners give preference to zirconia isomerization catalysts as they are more reliable and more efficient in operation;
- > Zirconia catalysts field of application has been widened: from C_5-C_6 isomerization to C_4 and C_7 isomerization.





MAIN ADVANTAGES OF C_5-C_6 FRACTIONS ISOMERIZATION TECHNOLOGIES ISOMALK-2

- ✓ Isomerate with octane number up to 92-93 RON and yield of 98% is produced
- ✓ Catalyst cycle length of 10 years and service life up to 12 years have been confirmed in practice
- \checkmark Catalyst is stable to the microimpurities of catalytic poisons

13 isomerization units Isomalk-2 have been commissioned by 2015, share of these units in Russian Federation is more than 50%



- ✓ Kogalymneftegaz (Russia), 15 KTA (III Q 2016);
- ✓ BPCL (Mumbai, India), 620 KTA (IV Q 2016)
- \checkmark PJSC TATNEFT (Russia), 420 KTA (IV Q 2016)
- Lifengda (China), 80 KTA (I Q 2017)
- ✓ HaiLinh HaiPhong Petroleum (Vietnam), 500 KTA (2017)
- ✓ KINEF Ltd. (Russia), 500 KTA (2018)
- Hengli (China), 2400 KTA (2018)







PJSC TATNEFT, NIZHNEKAMSK, RUSSIA ISOMERIZATION UNIT ISOMALK-2



OPERATING PERFORMANCES OF THE UNIT:

"Once-through" isomerization process scheme with low-branched hexanes recycle

Feed capacity, t/year	420,000
Isomerate yield, %	≥98
RON	≥91.2





KOGALYMNEFTEGAZ REFINERY, KOGALYM, RUSSIA PACKAGED ISOMERIZATION UNIT ISOMALK-2



OPERATING PERFORMANCES OF THE UNIT:

 "Once-through" isomerization process scheme with low-branched hexanes recycle

 Feed capacity, t/year
 15,200

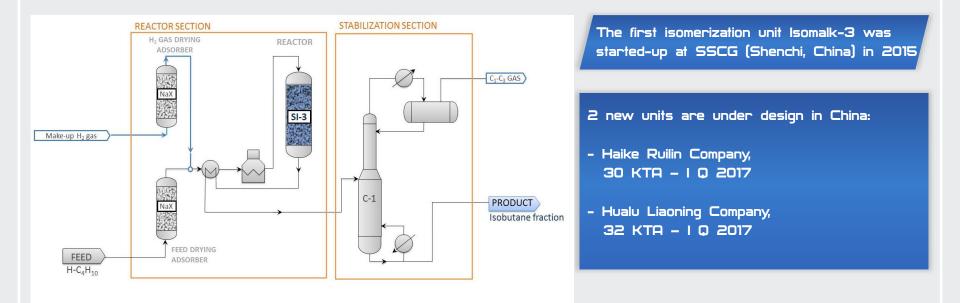
 Isomerate yield, %
 ≥95

 RON
 ≥88





N-BUTANE ISOMERIZATION TECHNOLOGY ISOMALK-3

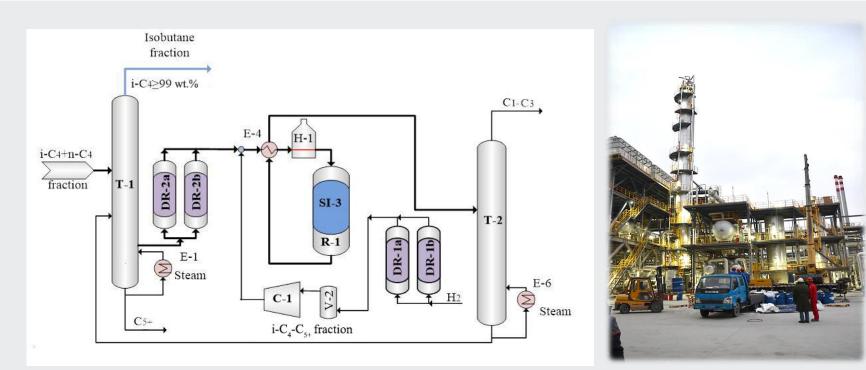


Typical n-butane isomerization unit Isomalk-3 consists of the following sections:

- **Isomerization feed treatment and drying section** is designed to remove moisture from isomerization feed; this operation is performed to protect catalyst against water, which suppresses catalyst activity;
- **Isomerization reactor section** is designed to perform isomerization reactions from normal butane to isobutane at the active sites of the catalyst at the most favorable conditions for the main reaction;
- **Hydrogen gas drying adsorbers section** is designed to remove moisture from hydrogen gas and from nitrogen during catalyst regeneration;
- Stabilizer section is designed to remove C_1 - C_3 hydrocarbons and dissolved hydrogen from obtained product.

SHANGDONG SINCIER PETROCHEMICAL CO., LTD, CHINA NEW ISOMERIZATION UNIT ISOMALK-3

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OPERATING PERFORMANCES OF THE UNIT:

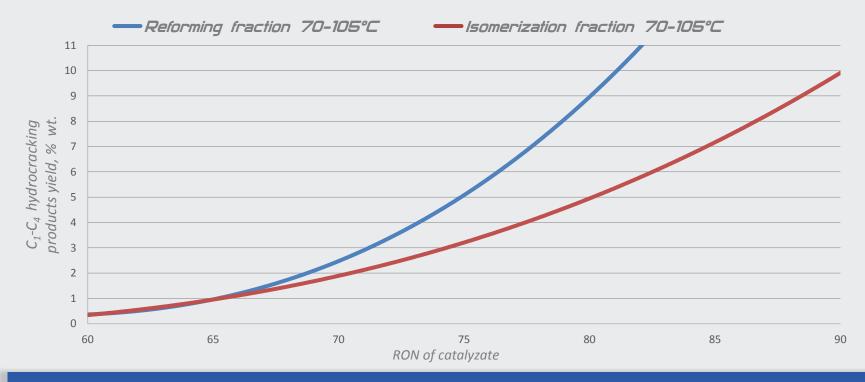
Isomerization process scheme with feed deisobutanization and n-butane recycle	
Feed capacity, t/year	200,000
C ₃ -C ₅ yield per n-C ₄ , %	<i>≥99</i>
H ₂ /HC molar ratio, mol/mol	0.06-0.1:1
Space velocity in reactor section, h ⁻¹	8-9



Parameter	Value
Temperature, °C	160-210
Pressure, MPag	1.5-2.0
Feed supply space velocity, hour ¹	6.0-8.0
H ₂ : butane molar ratio	0.07-0.10
"Once-through" n-butane conversion, % wt.	50-55
"Once-through" yield of C_3 + hydrocarbons, % wt.	99
"Once-through" yield of C_4 + hydrocarbons, % wt.	94-95
Total service life of the catalyst, years	no less than 8
Catalyst service cycle, years	no less than 3







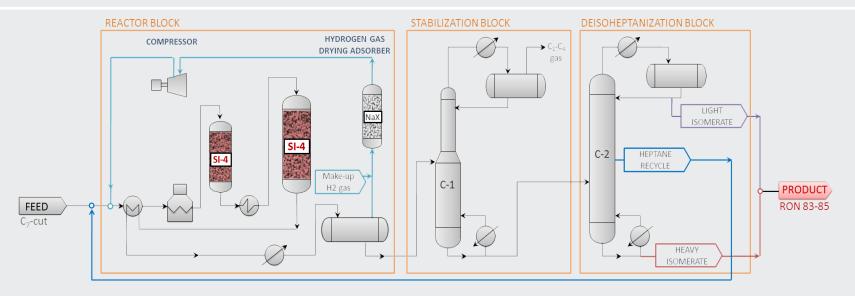
ADVANTAGES OF ISOMALK-4 TECHNOLOGY AGAINST REFORMING:

- ✓ Higher yield;
- No aromatic hydrocarbons in catalyzate;
- Decrease of expenses for MTBE and alkylate purchasing.





BASIC PROCESS FLOW-DIAGRAM OF ISOMALK-4 UNIT



CONDITIONS TO INCLUDE C7-FRACTION ISOMERIZATION UNIT TO THE GASOLINES PROCESSING SCHEME:

- Lack of alkylate and other high-octane non-aromatic motor gasoline components at refinery;
- Necessity to increase production of motor gasolines at the expense of higher selectivity of C₇-fraction processing.





CATALYTIC REFORMING OF GASOLINE FRACTIONS

There is no alternative to Platforming for obtaining high-octane motor gasoline component from heavy gasoline fraction 105-180°C yet. However, ever increasing ecological limitations of commercial motor gasolines compositions submit new even more severe requirements to the process:

For fixed-bed catalytic reforming units the challenge is issued to transfer to the catalysts being able to have service cycle of 3-4 years in severe mode (96-98 RON). In this case the reformate yield has to be equal to 88% and more.

For continuous catalytic reforming (CCR) unit the general requirements to catalysts are as follows: high selectivity together with high mechanical strength.





REFORMING CATALYSTS OF PJSC SIE NEFTEHIM



Reforming catalyst RC-12 for CCR units

High mechanical strength;High activity



New brand of reforming catalyst for fixed-bed units -REF-125

 Notably higher stability and selectivity in comparison with these of previous REF-23 series catalyst



CONCLUSION

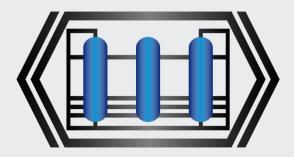
- The environmental requirements to motor gasolines are continued to be more severe in all countries;
- It is possible to meet the ecological requirements only in case of expansion of the processes, designed to produce high-octane non-aromatic motor gasoline components;
- General emphases are laid on the high-efficient isomerization technologies of C_5-C_6 fractions, n-butane, and C_7 -fraction;
- Russian refinery became one of the leaders in the sphere of construction of new isomerization units;
- Catalytic reforming remains one of the requested processes for production of motor gasolines and aromatic hydrocarbons, at this new more severe requirements are imposed;
- Researches for creation of new more efficient catalysts are conducted all over the world.





CONTACT INFORMATION OF PJSC SIE NEFTEHIM

THANK YOU FOR ATTENTION!



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