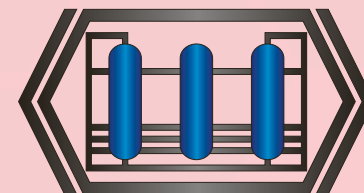


# **Enhancement of high quality motor gasoline production.**

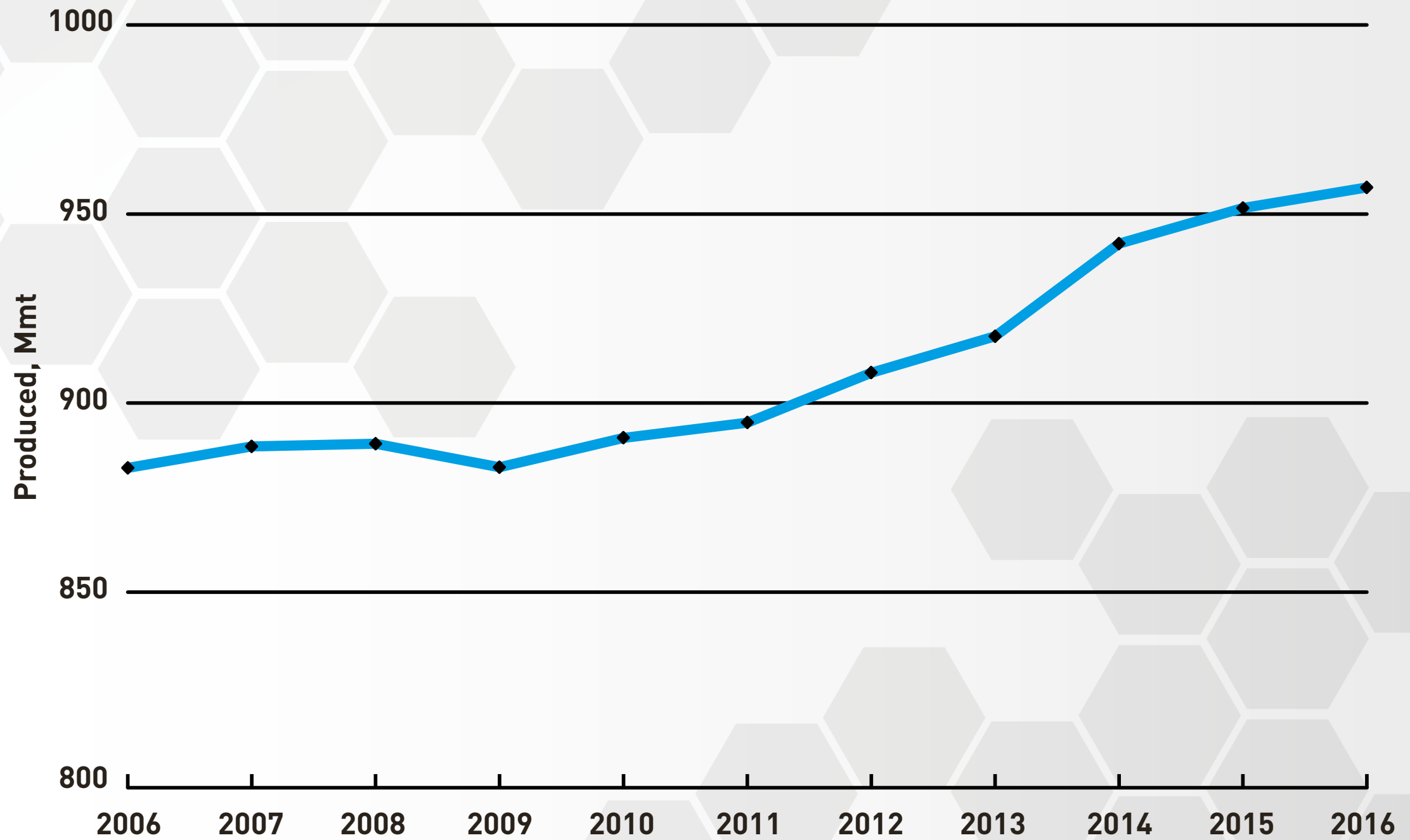
## **Under what conditions C7-cut isomerization is required?**

**Alexander Shakun, President and CEO, SIE Neftehim, LLC**

**17th Russia & CIS Refining Technology  
Conference & Exhibition - RRTC 2017**



## World trend of motor gasoline production



# Russian oil processing industry performances in 2012-2016

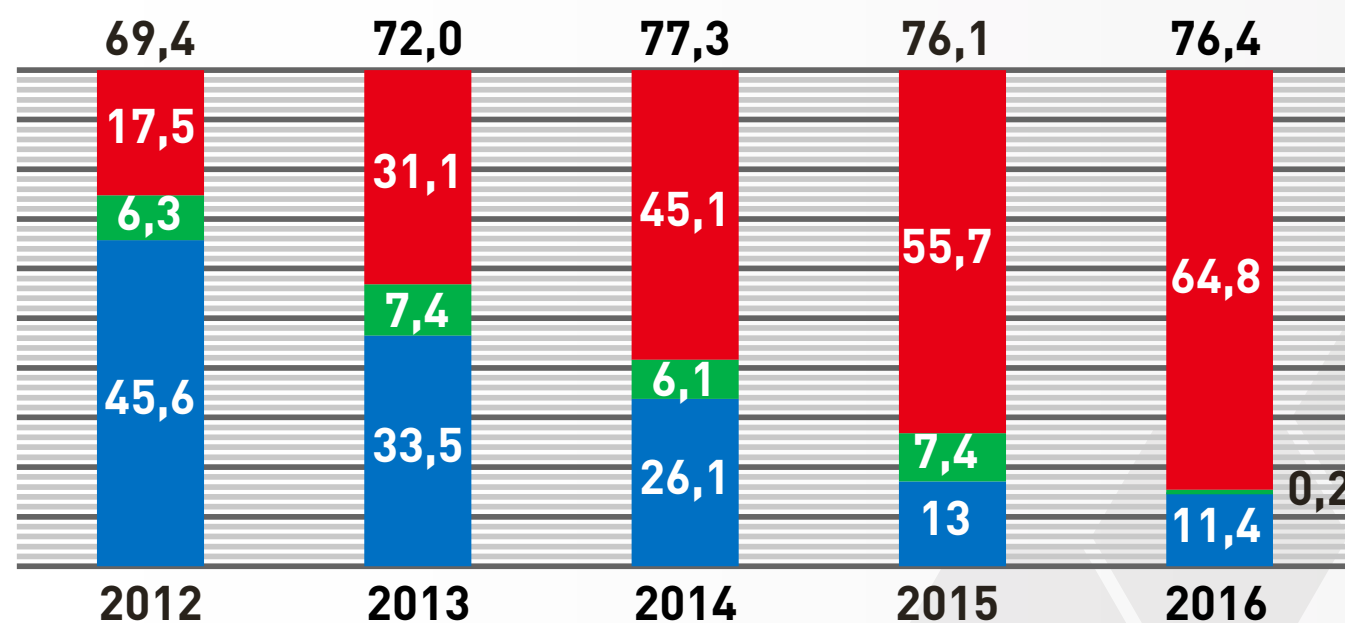
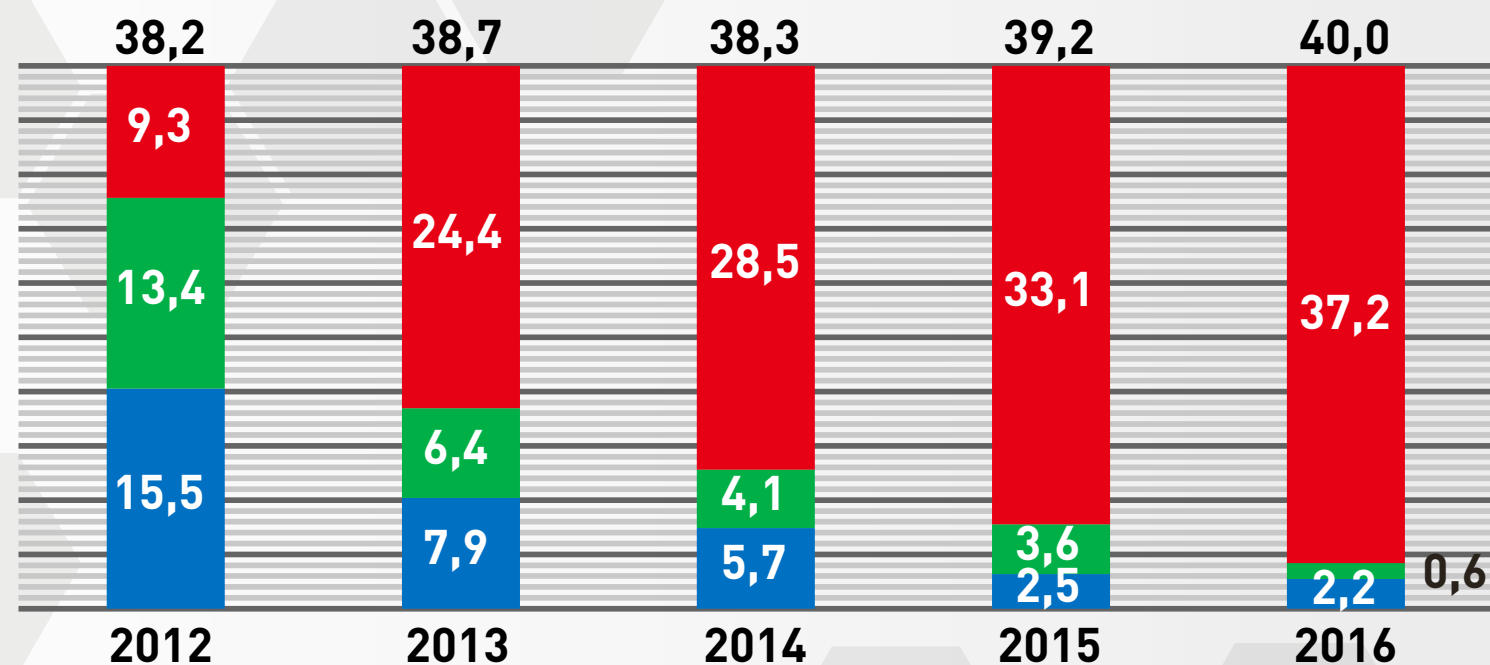
Motor gasoline production, MMt

2015-2016 Dynamics

K5 +4.1 MMt (+12.4%)

■ K3 and lower

■ K4 ■ K5



Diesel oil production, MMt

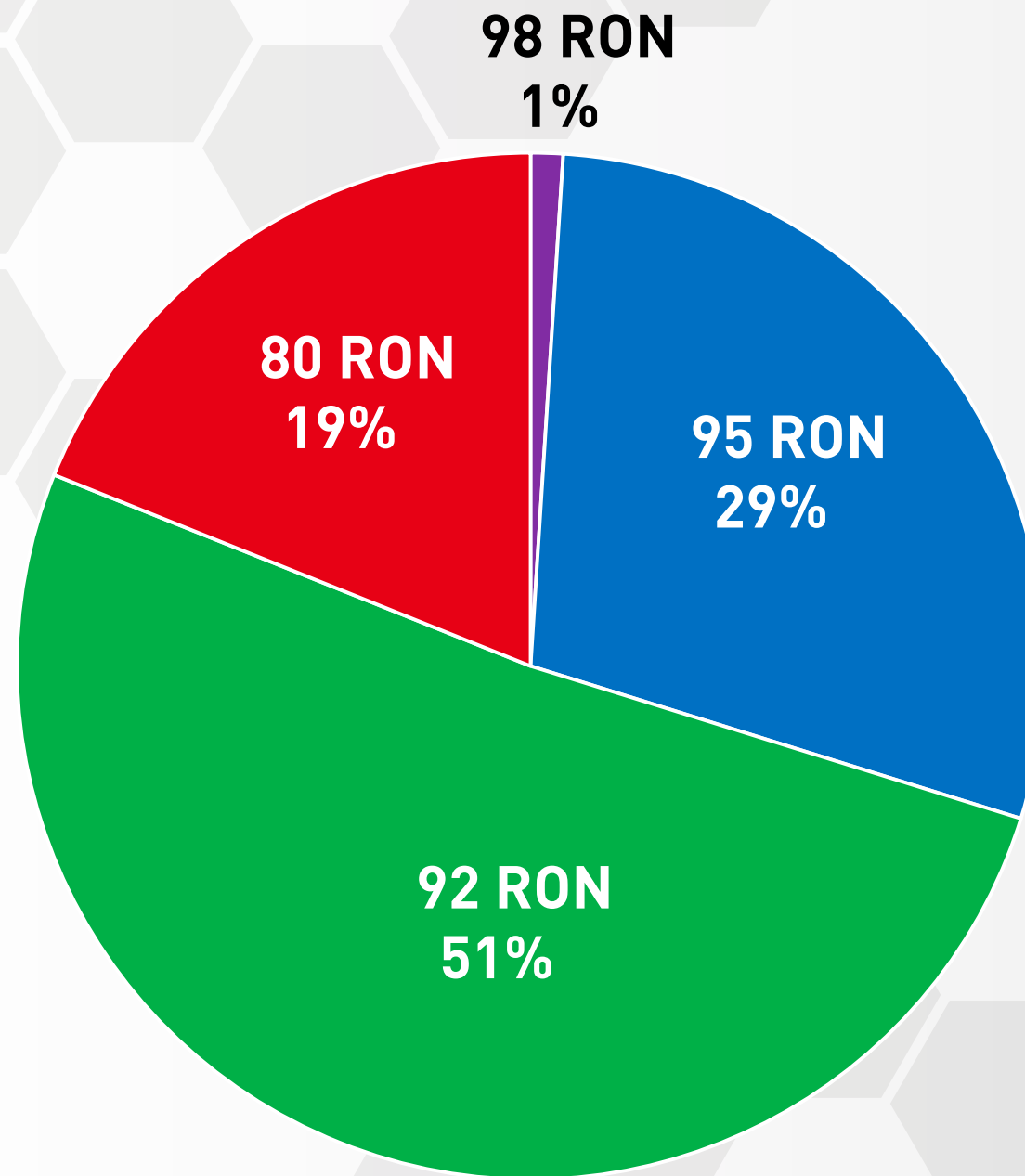
2015-2016 Dynamics

K5 +9.1 MMt (+16.3%)

■ K3 and lower

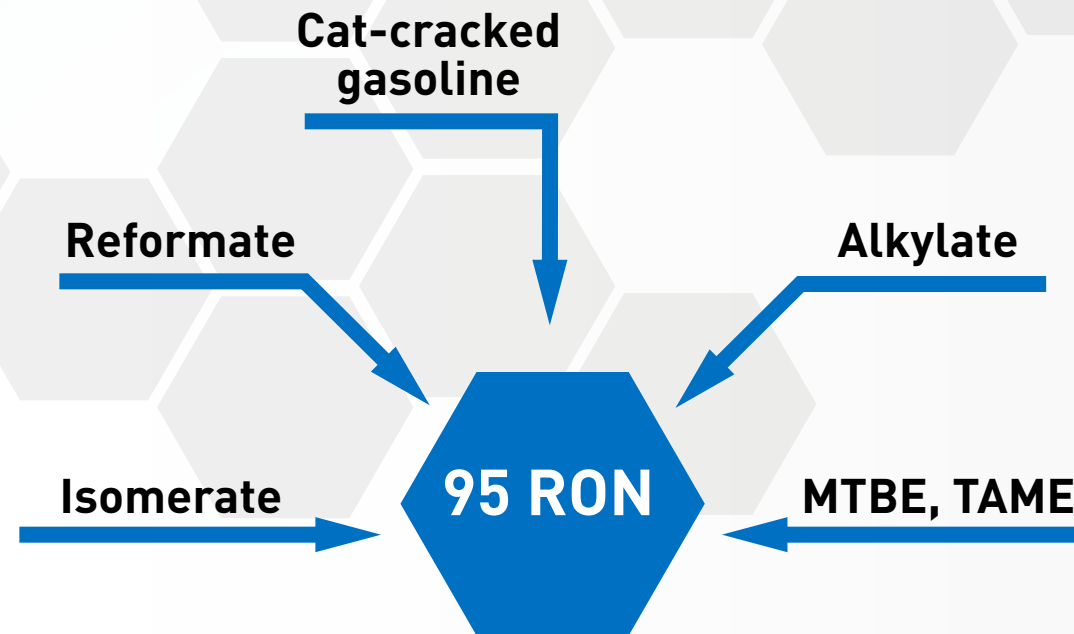
■ K4 ■ K5

**K5 environmental standard motor gasoline  
production in the first half of 2017  
in the Russian Federation**

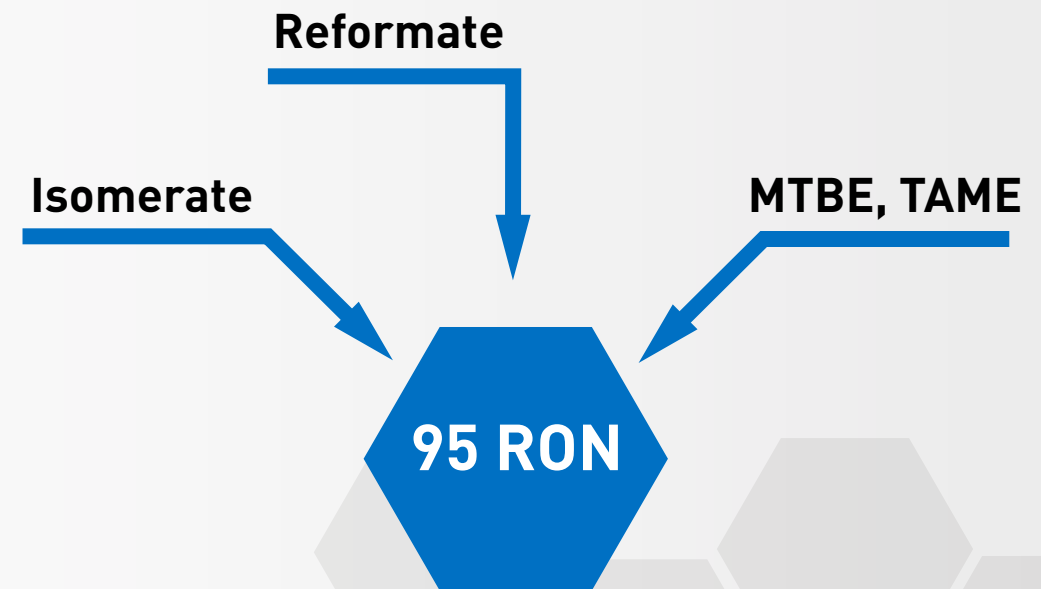


# Main arrangements of motor gasoline blending

## Option I



## Option II



## Disadvantages

### Option I

- High content of olefins and sulfur in cat-cracked gasoline
- Limited amount of alkylate

### Option II

- High content of aromatics due to high share of reformate

# CHALLENGES OF REFINERY IN MOTOR GASOLINE PRODUCTION

1. Deterioration of fixed-bed reformer performances due to catalyst coking and out-of-schedule shutdowns caused by poisoning.  
The share of fixed-bed reformers is still high

2. Out-of-schedule shutdowns of isomerization units due to highly-sensitive catalyst's poisoning and excessive corrosion

3. High share of reformate with increased aromatics content in motor gasoline production

## **Modern tasks of oil processing in production of high octane EURO-5 motor gasoline**

- ▶ **Increase of reforming catalysts' service cycle in fixed-bed reformers up to 3-4 years for "severe operation" with production of 97-99 RON reformat**
- ▶ **Enhancement of reformat yield in operating fixed-bed reformers up to 90-92% due to minimization of catalyst coking and pressure decrease**
- ▶ **Enhancement of CCR units operation due to improved catalyst selectivity and strength**
- ▶ **Increase of isomerization unit turnaround period up to 6 years**
- ▶ **Increase of period between regeneration for isomerization units up to 12 years**
- ▶ **Maximization of non-aromatic isomerate share by means of C<sub>7</sub>-cut redistribution from reforming feed to isomerization feed**
- ▶ **Construction of n-butane isomerization units to obtain feed for alkylate and MTBE production**

## Recent modifications of reforming catalysts produced and supplied by SIE NEFTEHIM, LLC

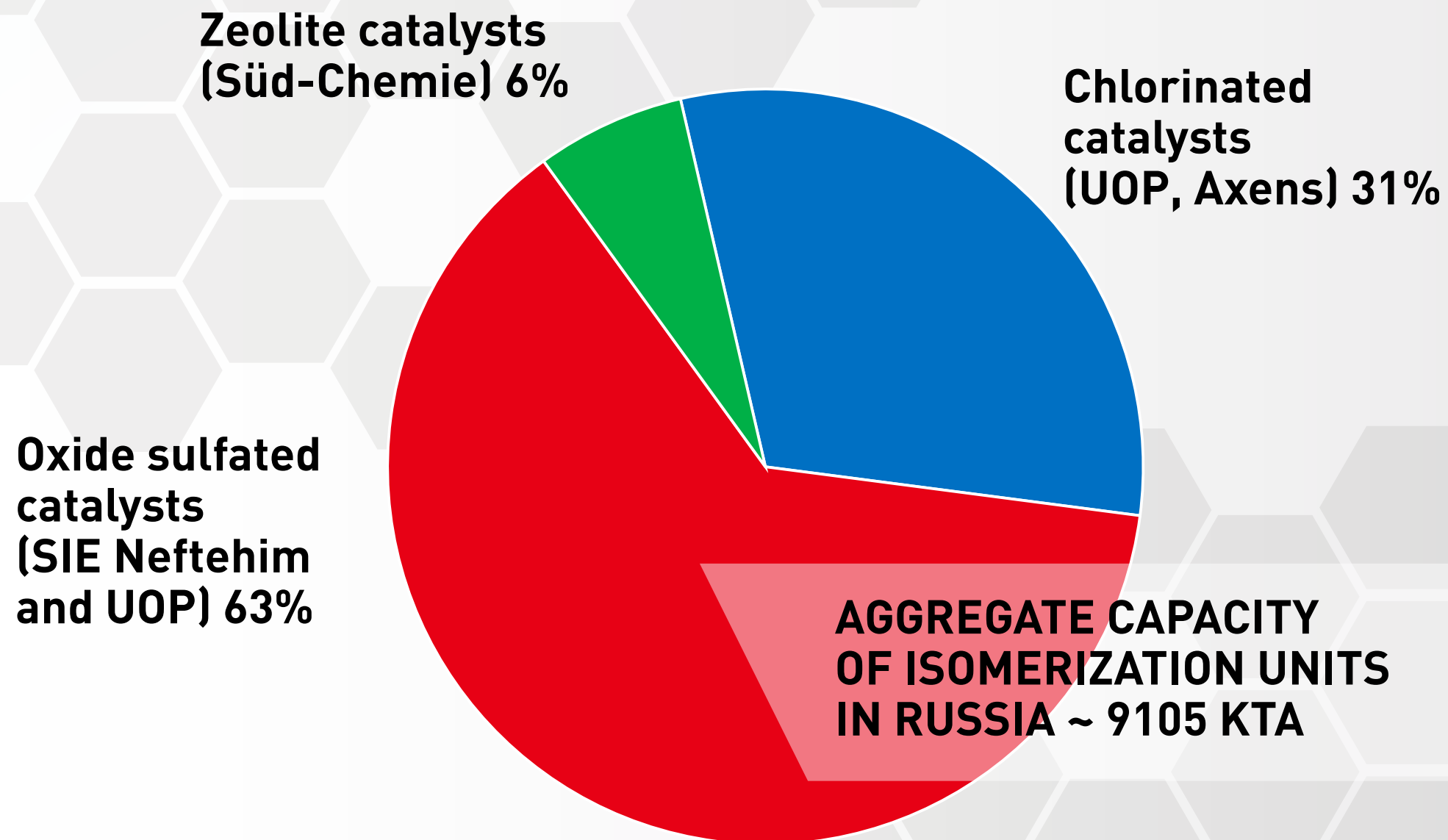
BRAND	SERVICE	MODE	SERVICE CYCLE	SERVICE LIFE	REFORMATE YIELD
REF	Fixed-bed	Up to 100 RON	Up to 4 years	Not less than 8 years	Up to 90%
RC	CCR	Up to 110 RON	-	Not less than 8 years	Up to 92%

### Factors, determining catalytic properties of reforming catalysts

- ▶ Physical and chemical properties of catalyst support
- ▶ Loading conditions for platinum, promoters, and modifiers
- ▶ Conditions of drying and calcination
- ▶ Activation conditions in a reforming unit
- ▶ Conditions of reformer feed preparation
- ▶ Management of all production and operation stages for reforming catalyst (scientific and technical support)



## SHARE OF DIFFERENT ISOMERIZATION TECHNOLOGIES IN RUSSIA



## **BENEFITS OF OXIDE SULFATED ISOMERIZATION CATALYSTS**

- ▶ **Long-term service life and service cycle**
- ▶ **Possible activity restoration via regeneration**
- ▶ **Tolerance to H<sub>2</sub>O and sulfur traces**
- ▶ **Low corrosiveness**

- ▶ **12 years service life has been achieved over SI-2 catalyst**
- ▶ **12 years service cycle without regeneration has been achieved over SI-2 catalyst**
- ▶ **Catalyst SI-2 totally restores its activity after removal of impurities from feed and hydrogen gas**

## **Commercial introduction of n-butane isomerization process based on oxide sulfated catalyst**

**2015**

**200 KTA Isomalk-3 unit, Shandong Sincier Petrochemical Co., Ltd (China), a part of MTBE complex**

**2016- 2017**

**Construction and start-up of 2 new Isomalk-3 units in China**

**2017- ...**

**Technology promotion in different countries**

# Isomalk-3 unit, Shandong Sincier Petrochemical Co., Ltd





## **C<sub>7</sub>-cut (70-105°C) isomerization process Isomalk-4**



**Octane number enhancement for 70-105°C straight run cut from 65 up to 85 numbers and complete hydrogenation of aromatics**



**Recovery of 70-105°C cut from reformer feed allows for increasing the reformate yield and octane**



**Involvement of 70-105°C cut isomerization into processing circuit allows for producing EURO-5 motor gasoline without addition of alkylate and cat-cracked gasoline**

# CONCLUSION

## **1. Efficiency improvement of high octane EURO-5 motor gasoline production requires enhancement of naphtha processing technologies in the following ways:**

- ▶ **Creation of catalysts for fixed-bed units with long-term service cycle (up to 4 years) for «severe» operation (up to 99-100 octane numbers).**
- ▶ **Creation of CCR reforming catalysts with enhanced mechanical strength and selectivity.**
- ▶ **Further increase of pentane-hexane isomerization units' share based on oxide sulfated catalysts, providing unit service cycle up to 6 years and more.**
- ▶ **Construction of n-butane isomerization units to provide feed for alkylation and MTBE units. New technology Isomalk-3 providing stable unit operation has been introduced.**
- ▶ **Transfer of 70-105°C cut from reformers to isomerization units for refineries with limited alkylate amount. C7-cut isomerization technology Isomalk-4 has been developed.**

## **2. All necessary technologies for production of EURO-5 motor gasoline are developed in Russia.**

# THANK YOU!



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